FIG. 1.

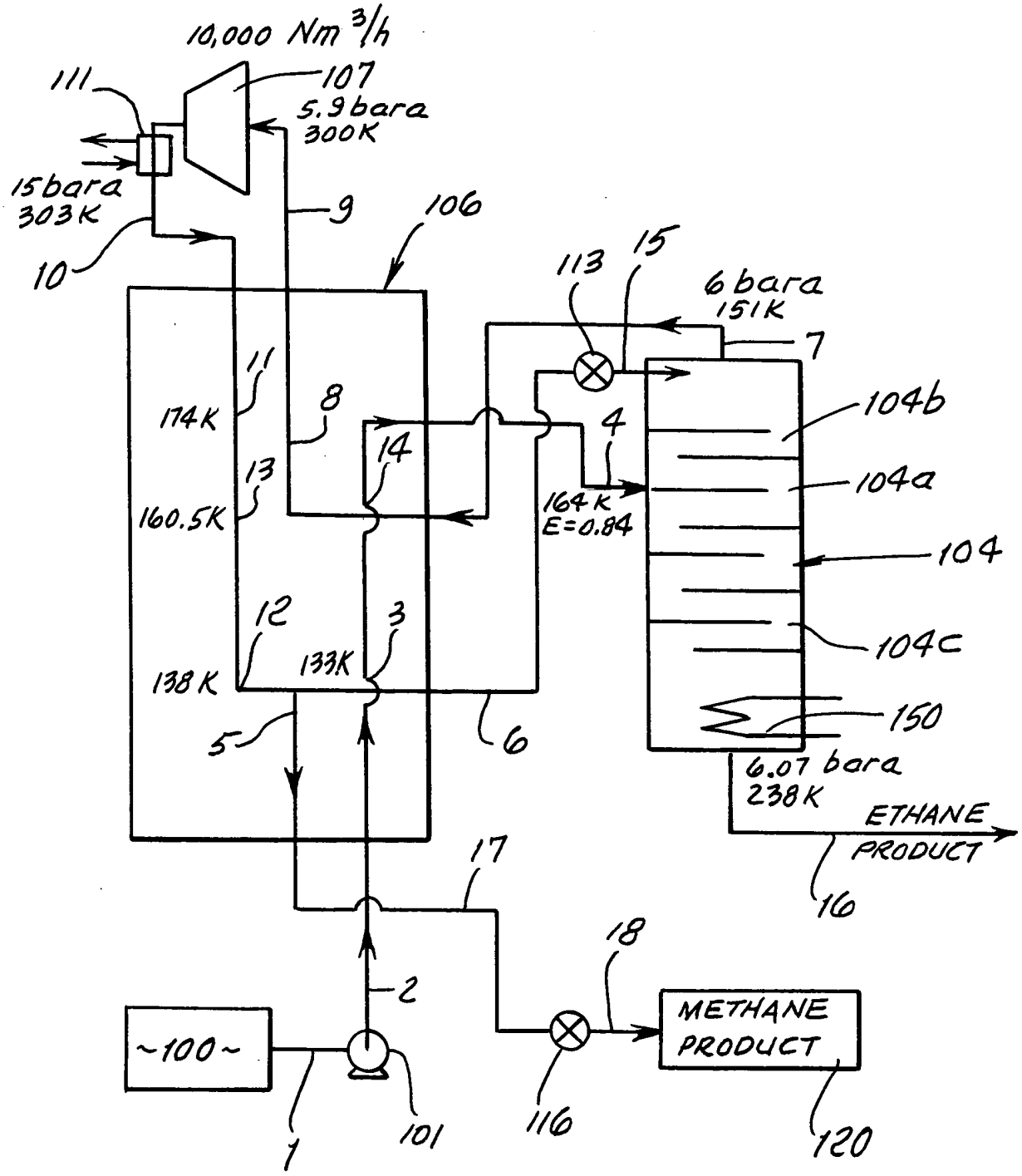

Fig. 1a.

TABLE 1

	Initial	Methane Product	Ethane Product
Flow rate, Nm^3/b	**10000**	**8755**	**1245**
Pressure, bara/paia	**1.05/15.2**	**1.35/19.6**	**6.07/88.0**
Temperature K	**112.6**	**114.6**	**238**
Vapor Mole Fraction	**0.0**	**0.0**	**0.0**
Component mole fraction			
- nitrogen	**0.003**	**0.00343**	**0.0**
- methane	**0.858**	**0.98**	**0.0**
- ethane	**0.096**	**0.01657**	**0.6546**
- propane	**0.030**	**0.0**	**0.2410**
- I-butane	**0.010**	**0.0**	**0.0803**
- I-pentane	**0.002**	**0.0**	**0.0161**
- n-hexane	**0.001**	**0.0**	**0.0080**

FIG. 1b.

TABLE 2

The parameters of the scheme of the LNG enriching plant according to the Figure 1 (the distillation column pressure is 6 bara (87 psia)

No	Flow rate V. mol/mol LNG	Temperature T. K	Pressure P bara	Vapor mole fraction E.	Composition (see Fig. 1a)
1	1.0	112.6	1.05	0.0 sat.	Initial LNG
2	1.0	112.9	6.1	0.0	Initial LNG
3	1.0	132.4	6.09	0.0	Initial LNG
4	1.0	164.0	6.03	0.84	Initial LNG
5	0.8755	138.0	14.9	0.0	Methane product
6	0.1245	138.0	14.9	0.0	Methane product
7	1.0	151.4	6.0	1.0 sat.	Methane product
8	1.0	164.0	5.95	1.0	Methane product
9	1.0	300.0	5.9	1.0	Methane product
10	1.0	303.0	15.0	1.0	Methane product
11	1.0	174.1	14.95	1.0	Methane product
12	1.0	138.0	14.9	0.0	Methane product
13	1.0	160.5	14.93	0.79	Methane product
14	1.0	151.4	6.07	0.72	Initial LNG
15	0.1245	138.2	6.0	0.0	Methane product
16	0.1245	238.0	6.07	0.0 sat.	Ethane product
17	0.8755	114.6	14.85	0.0	Methane product
18	0.8755	114.6	1.35	0.0 sat.	Methane product

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Replacement sheet

FIG. 1C.

The Temperature (T) of the streams in the heat exchanger vs. Enthalpy (H) of the Direct streams.
To Fig 1: the distillation column pressure is 6.0 bara (87.0 psia).

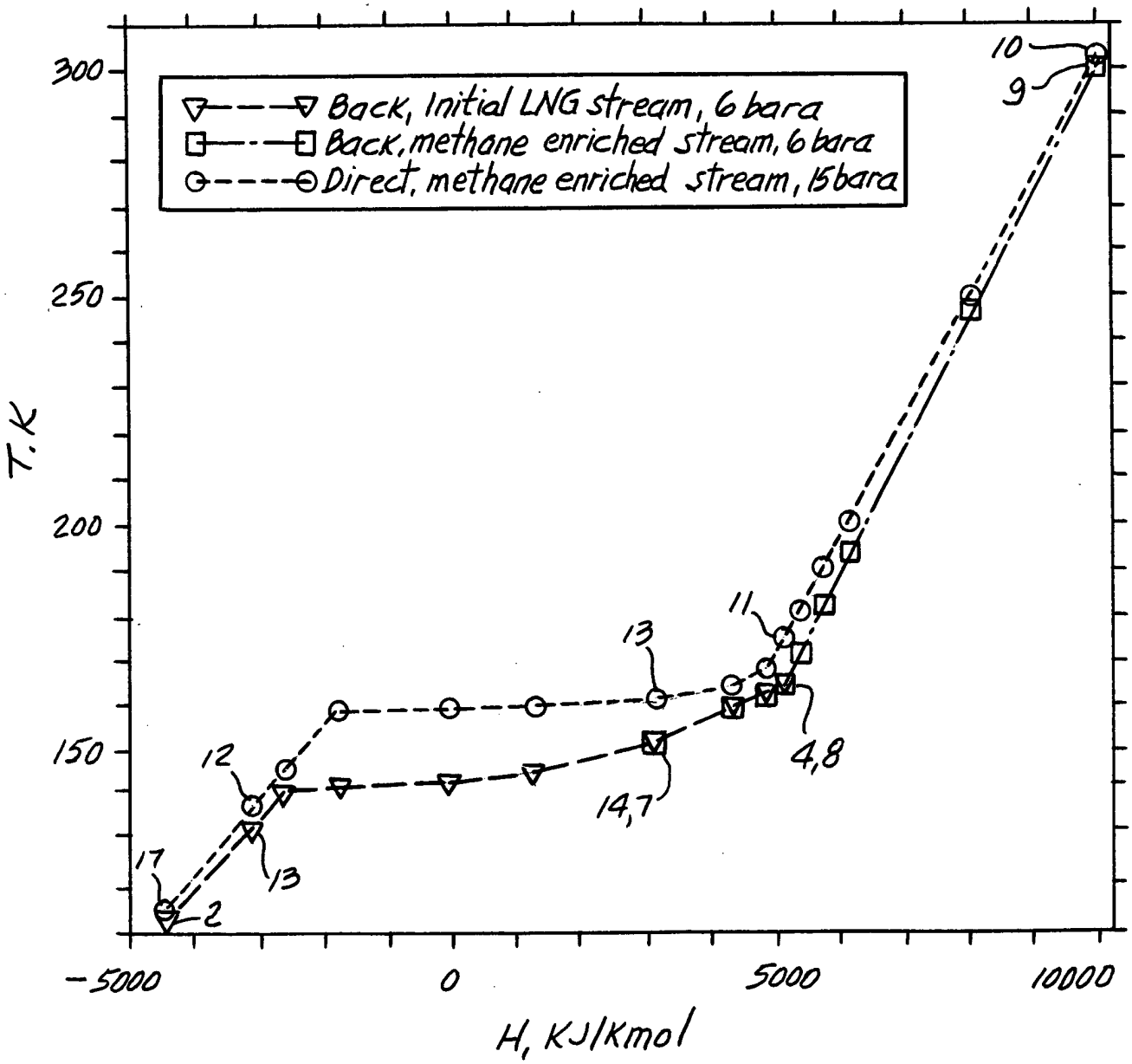

FIG. 2.

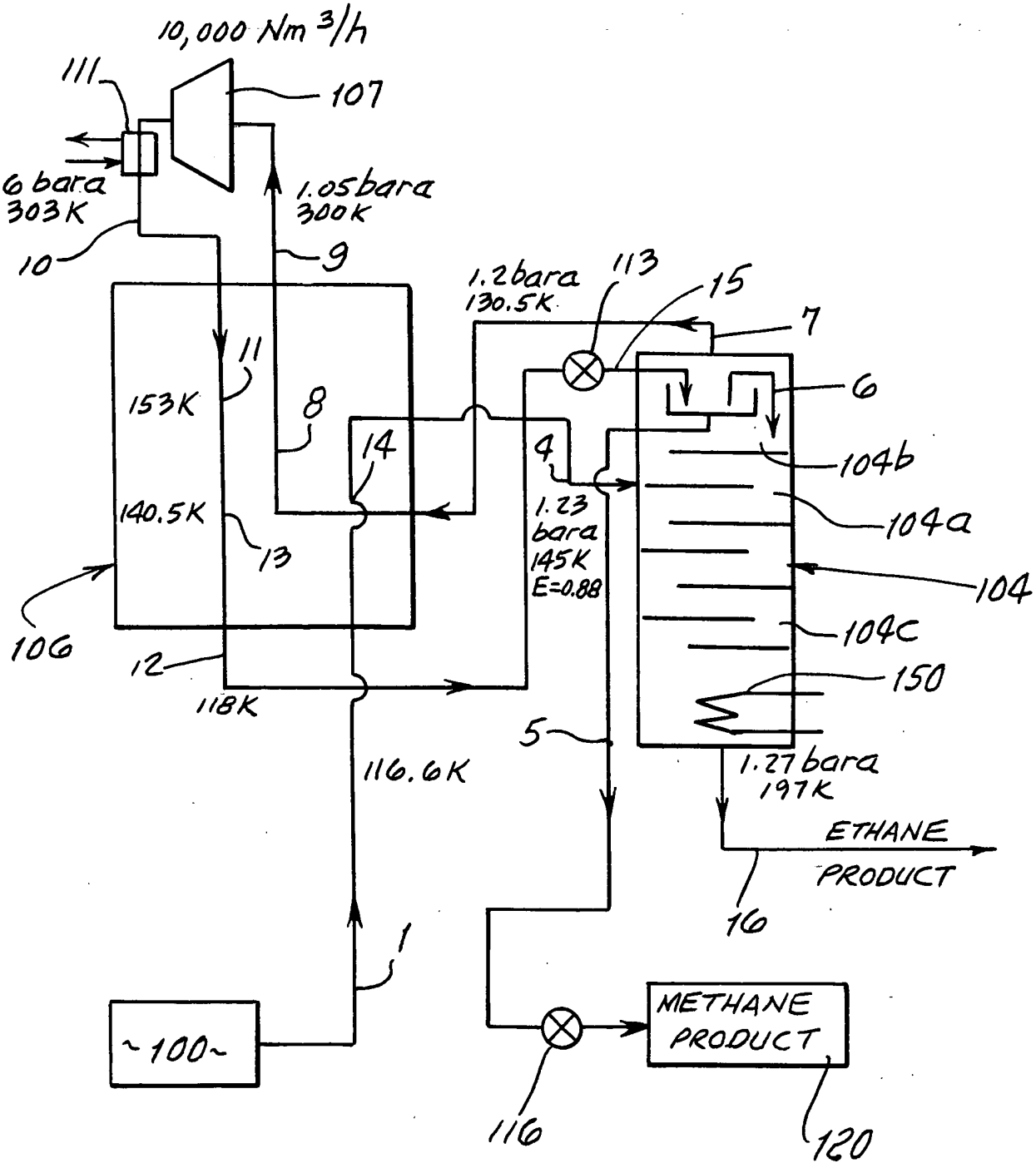
10,000 Nm³/h
111
107
6 bara
303K
1.05bara
300K
10
9
1.2bara
130.5K
113
15
7
11
153K
8
14
6
104b
4
140.5K
13
1.23
bara
145K
E=0.88
104a
104
106
12
118K
104c
150
5
116.6K
1.27bara
197K
ETHANE
PRODUCT
16
1
~100~
METHANE
PRODUCT
116
120

FIG. 2a.

TABLE 3

	Initial	Methane Product	Ethane Product
Flow rate, Nm^3/b	10000	8755	1245
Pressure, bara/paia	1.4/20.3	1.2/17.4	1.27/18.4
Temperature K	116.6	113.1	197
Vapor Mole Fraction	0.0	0.0	0.0
Component mole fraction			
- nitrogen	0.003	0.00343	0.0
- methane	0.858	0.98	0.0
- ethane	0.096	0.01657	0.6546
- propane	0.030	0.0	0.2410
- I-butane	0.010	0.0	0.0803
- I-pentane	0.002	0.0	0.0161
- n-hexane	0.001	0.0	0.0080

Fig. 2b.

TABLE 4

The parameters of the scheme of the LNG enriching plant according to the Figure 2 (the distillation column pressure is 1.2 bara (17.4 psia)

No	Flow rate V, mol/mol LNG	Temperature T, K	Pressure P, bara	Vapor mole fraction E,	Composition (see Fig.2a)
1	1.0	116.6	1.4	0.0 sat.	Initial LNG
4	1.0	145.2	1.23	0.88	Initial LNG
5	0.8755	113.1	1.2	0.0 sat.	Methane product
6	0.091	113.1	1.2	0.0 sat.	Methane product
7	1.0	130.5	1.2	1.0 sat.	Methane product
8	1.0	145.2	1.15	1.0	Methane product
9	1.0	300.0	1.05	1.0	Methane product
10	1.0	303.0	6.0	1.0	Methane product
11	1.0	153.1	5.95	1.0	Methane product
12	1.0	118.0	5.9	0.0	Methane product
13	1.0	140.5	5.93	0.82	Methane product
14	1.0	130.5	1.3	0.81	Initial LNG
15	1.0	113.4	1.2	0.034	Methane product
16	0.1245	197.0	1.27	0.0 sat.	Ethane product

FIG. 2C.

The Temperature (T) of the streams in the heat exchanger vs. Enthalpy (H) of the Direct streams. To Fig. 2: the distillation column pressure is 1.2 bara (17.4 psia).